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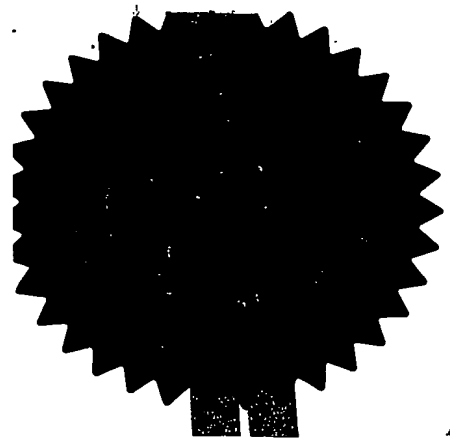
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Patents Form 1/77 8 MAR 2002

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Cardiff Road  
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## Request for grant of a patent

1. Your Reference APB/GRK/M10553

2. Application number

28 MAR 2002

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3. Full name, address and postcode  
of the or each ApplicantAdvanced Gel Technology Limited  
Unit 41 Campus Road  
Listerhills Science Park  
Bradford  
BD7 1HRCountry/state of incorporation  
(if applicable)Aubin Limited  
Unit 1, Castle Street  
Castle Park Industrial Estate

Incorporated in: United Kingdom

4. Title of the invention

RECOVERING MATERIALS

5. Name of agent

APPLEYARD LEES

Address for service in the UK to  
which all correspondence should  
be sent15 CLARE ROAD  
HALIFAX  
HX1 2HY

Patents ADP number

190001

6. Priority claimed to:

Country

Application number

Date of filing

7. Divisional status claimed from:

Number of parent application

Date of filing

8. Is a statement of inventorship and  
of right to grant a patent required in  
support of this application?

YES

## Patents Form 1/77

Page 2/2

9. Enter the number of sheets for any of the following items you are filing with this form. Do not count copies of the same document

Continuation sheets of this form

Description

24

Claim(s)

Abstract

Drawing(s)

1 only

10. If you are also filing any of the following, state how many against each item

Priority documents

Translation of priority documents

Statement of inventorship and right to grant a patent (PF 7/77)

Request for a preliminary examination and search (PF 9/77)

Request for a preliminary examination (PF 10/77)

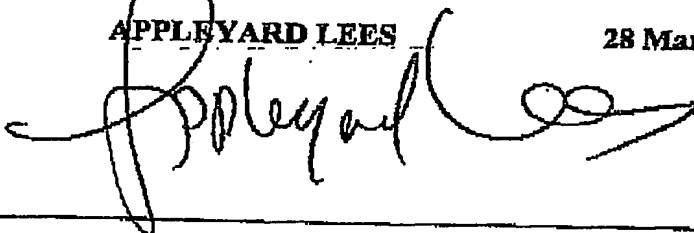
Any other documents (please specify)

11.

We request the grant of a patent on the basis of this application.  
Signature Date

APLEYARD LEES

28 March 2002



12. Contact

Anthony P Brierley- 01422 330110

Recovering Materials

This invention relates to a process for recovering materials and particularly, although not exclusively, relates to a process for recovering materials, for example organic fluids such as oil, tar or gas from a subterranean reservoir.

Organic fluids, such as oil found within a subterranean formation, for example in a reservoir, are recovered via production wells which are drilled into the subterranean formulation. Generally a large amount of oil is left in the formation after recovery by primary recovery methods which utilize only the natural forces present in the formation for forcing oil into the production wells. Where the initial formation energy is inadequate or become depleted through production from the well, supplementary processes referred to as secondary, tertiary and quaternary recovery operations are utilized in order to recover a larger percentage of the oil.

Known secondary recovery techniques include steam flooding and water flooding. In these techniques, steam or water is injected into an injection well spaced from a production well. The injected fluid forces oil within the formation to move towards the production well from which it may be recovered.

Tertiary recovery process utilise chemicals to further increase the efficiency of the removal of oil from oil bearing layers. The known chemicals used have generally been of two types. The first comprises a surfactant or like product which alters the oil/water/rock surface

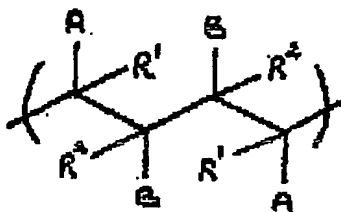
tension. The second type is relatively viscous and provides an increased viscosity which will slow the passage of water through a rock matrix and push any freed oil out. Additionally, substances such as carbon dioxide have been used to assist with the oil removal process leading to higher oil removal from subterranean formations.

In view of the value of oil and the potential financial rewards available if the amounts removed can be increased economically, there are large numbers of patents and other publications which describe so called "enhanced oil-recovery techniques". Many of the techniques described however, still suffer from significant disadvantages. For example the use of surfactants can lead to a change in the wettability of oil-bearing formations which can potentially damage reservoirs. Furthermore, surfactants are often of low viscosity and therefore inefficient "pushers" of oil through formations. Additionally, surfactants may not be heat stable or may otherwise be affected by the temperatures (up to 180°C) or pressures (20000-30000 psi) to which they can be subjected in use.

It is an object of the present invention to address problems associated with recovery of organic fluids from subterranean formations, especially with tertiary oil recovery.

According to a first aspect of the invention, there is provided a process for recovering materials from a subterranean formation, for example a reservoir, the process comprising:

(a) selecting a first polymeric material having a repeat unit of formula



wherein A and B are the same or different, are selected from optionally-substituted aromatic and heteroaromatic groups and at least one comprises a relatively polar atom or group and R<sup>1</sup> and R<sup>2</sup> independently comprise relatively non-polar atoms or groups;

(b) selecting a second polymeric material which includes a functional group which is able to react in the presence of said first polymeric material to form a third polymeric material;

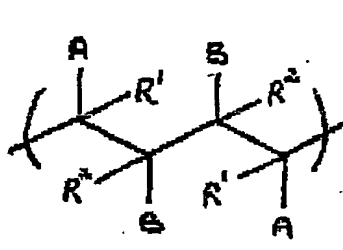
(c) causing the formation of said third polymeric material by a reaction involving said first and second polymeric materials; and

(d) contacting the subterranean formation with said third polymeric material.

According to a second aspect of the invention, there is provided a process for recovering materials from a subterranean formation for example a reservoir, the process comprising contacting the formation with a polymeric material (herein "said third polymeric material") which is a product of a reaction involving

(a) a first polymeric material having a repeat unit of formula

5



10 wherein A and B are the same or different, are selected from optionally-substituted aromatic and heteroaromatic groups and at least one comprises a relatively polar atom or group and R<sup>1</sup> and R<sup>2</sup> independently comprise relatively non-polar atoms  
15 or groups; and

20 a second polymeric material which includes a functional group which is able to react in the presence of said first polymeric material to form said third polymeric material.

A and/or B could be multi-cyclic aromatic or heteroaromatic groups. Preferably, A and B are independently selected from optionally-substituted five or more preferably six-  
25 membered aromatic and heteroaromatic groups. Preferred heteroatoms of said heteroaromatic groups include nitrogen, oxygen and sulphur atoms of which oxygen and especially nitrogen, are preferred. Preferred heteroaromatic groups include only one heteroatom. Preferably, a or said  
30 heteroatom is positioned furthest away from the position of attachment of the heteroaromatic group to the polymer backbone. For example, where the heteroaromatic group comprises a six-membered ring, the heteroatom is preferably provided at the 4-position relative to the position of the  
35 bond of the ring with the polymeric backbone.

Preferably, A and B represent different groups. Preferably, one of A or B represents an optionally-substituted aromatic group and the other one represents an optionally-substituted heteroaromatic group. Preferably A represents an optionally-substituted aromatic group and B represents an optionally-substituted heteroaromatic group especially one including a nitrogen heteroatom such as a pyridinyl group.

10

Unless otherwise stated, optionally-substituted groups described herein, for example groups A and B, may be substituted by halogen atoms, and optionally substituted alkyl, acyl, acetal, hemiacetal, acetalalkyloxy, hemiacetalalkyloxy, nitro, cyano, alkoxy, hydroxy, amino, alkylamino, sulphinyl, alkylsulphinyl, sulphonyl, alkylsulphonyl, sulphonate, amido, alkylamido, alkylcarbonyl, alkoxy carbonyl, halocarbonyl and haloalkyl groups. Preferably, up to 3, more preferably up to 1 optional substituents may be provided on an optionally substituted group.

15  
20

Unless otherwise stated, an alkyl group may have up to 10, preferably up to 6, more preferably up to 4 carbon atoms, with methyl and ethyl groups being especially preferred.

25

Preferably, A and B each represent polar atoms or group -that is, there is preferably some charge separation in groups A and B and/or groups A and B do not include carbon and hydrogen atoms only.

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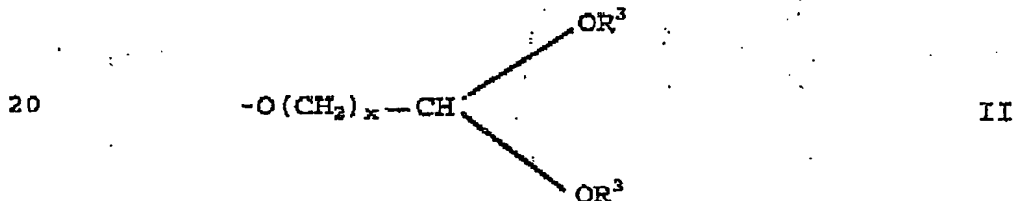
Preferably, at least one of A or B includes a functional group which can undergo a condensation reaction, for example on reaction with said second polymeric material.



~~Preferably, A includes a said functional group which can undergo a condensation reaction.~~

Preferably, one of groups A and B includes an optional  
5 substituent which includes a carbonyl or acetal group with  
a formyl group being especially preferred. The other one  
of groups A and B may include an optional substituent which  
is an alkyl group, with an optionally substituted,  
10 preferably unsubstituted, C<sub>1-4</sub> alkyl group, for example a  
methyl group, being especially preferred.

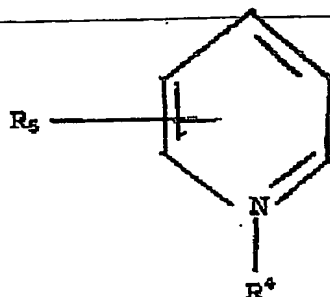
Preferably, A represents a group, for example an aromatic  
group, especially a phenyl group, substituted (preferably  
at the 4-position relative to polymeric backbone when A  
15 represents an optionally-substituted phenyl group) by a  
formyl group or a group of general formula



where x is an integer from 1 to 6 and each R<sup>3</sup> is  
25 independently an alkyl or phenyl group or together form an  
alkylene group.

Preferably, B represents an optionally-substituted  
heteroaromatic group, especially a nitrogen-containing  
30 heteroaromatic group, substituted on the heteroatom with a  
hydrogen atom or an alkyl or aralkyl group. More  
preferably, B represents a group of general formula

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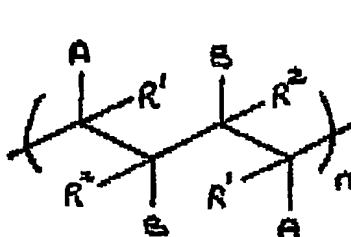
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wherein  $R^4$  represents a hydrogen atom or an alkyl or aralkyl group,  $R^5$  represents a hydrogen atom or an alkyl group and  $X^-$  represents a strongly acidic ion.

Preferably,  $R^1$  and  $R^2$  are independently selected from a hydrogen atom or an optionally-substituted, preferably unsubstituted, alkyl group. Preferably,  $R^1$  and  $R^2$  represent the same atom or group. Preferably,  $R^1$  and  $R^2$  represent a hydrogen atom.

Preferred first polymeric materials may be prepared from any of the compounds described on page 3 line 8 to line 39 of GB2030575B by the method described in WO98/12239 and the contents of the aforementioned documents are incorporated herein by reference.

Said first polymeric material may be of formula



wherein  $A$ ,  $B$ ,  $R^1$  and  $R^2$  are as described above and  $n$  is an integer. Integer  $n$  is suitably 10 or less, preferably 8 or less, more preferably 6 or less, especially 5 or less.

~~Integer n is suitably at least 1, preferably at least 2,~~  
more preferably at least 3. Preferably, formation of said  
third polymeric material from said first and second  
polymeric materials involves a condensation reaction.

- 5 Preferably, formation of said third polymeric material  
involves an acid catalysed reaction. Preferably, said  
first and second polymeric materials include functional  
groups which are arranged to react, for example to undergo  
a condensation reaction, thereby to form said third  
10 polymeric material. Preferably, said first and second  
polymeric materials include functional groups which are  
arranged to react for example to undergo an acid  
catalysed reaction thereby to form said third polymeric  
material.

15

- Preferably, said second polymeric material includes a  
functional group selected from an alcohol, carboxylic acid,  
carboxylic acid derivative, for example an ester, and an  
amine group. Said second polymeric material preferably  
20 includes a backbone comprising, preferably consisting  
essentially of carbon atoms. The backbone is preferably  
saturated. Pendent from the backbone are one or more said  
functional groups described. Said polymer may have a  
molecular weight of at least 10,000. Said second polymeric  
25 material is preferably a polyvinyl polymer. Preferred  
second polymeric compounds include optionally substituted,  
preferably unsubstituted, polyvinylalcohol,  
polyvinylacetate, polyalkylene glycols, for example  
polypropylene glycol, and collagen (and any component  
30 thereof).

- Suitably, a mixture comprising 0.3wt% or less, preferably  
0.25 wt% or less, more preferably 0.2 wt% or less of said  
first polymeric material is used in the preparation of  
35 said third polymeric material. Suitably, said mixture  
includes 3wt% or less, preferably 2.5wt% or less, more

preferably 2wt% or less of said second polymeric material.

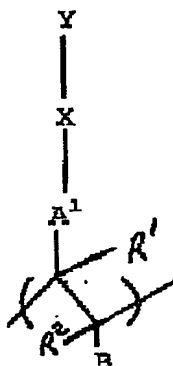
Preferably, said mixture includes a solvent, especially water. Said mixture may include at least 80wt%, suitably includes at least 85wt%, preferably includes at least 5 92wt%, more preferably includes at least 95wt%, especially includes at least 98wt% water. Said mixture may include other minor components, for example a catalyst, especially an acid, for catalysing the formation of said third polymeric material from said first and second polymeric 10 materials. In some cases, said water may be derived from sea water and, accordingly, said mixture may include salts (e.g. sodium chloride) and other components found in sea water. In general terms water for use as described herein may be derived from any convenient source. It may be 15 potable water, surface water, sea water, aquifer water, deionised production water and filtered water derived from any of the aforementioned sources. The water may be treated so that it is suitable for use as an injection fluid. For example, it may be treated by addition of 20 oxygen scavengers, biocides, corrosion inhibitors, scale inhibitors, anti-foaming agents and flow improvers. Sea water and/or water from other sources may be deoxygenated and/or desulphonated.

25 Said mixture suitably includes at least 0.0001 wt%, preferably at least 0.001wt%, more preferably at least 0.01 wt%, especially at least 0.05wt% of said first polymeric material. Said mixture suitably includes at least 0.01wt%, preferably at least 0.1wt%, more preferably 30 at least 1wt% of said second polymeric material.

Said third polymeric material suitably includes a moiety of formula

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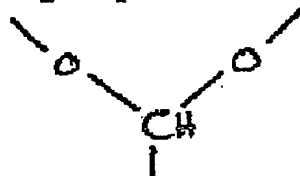
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wherein R<sup>1</sup>, R<sup>2</sup> and B are as described above, A<sup>1</sup> represents a residue of group A described above after the reaction involving said first and second polymeric materials, Y represents a residue of said second polymeric material after said reaction involving said first and second polymeric materials and X represents a linking group or group extending between the residues of said first and second polymeric materials. In one preferred embodiment A<sup>1</sup> represents an optionally-substituted phenyl group, X represents a group

20



25

which is bonded via the oxygen atoms to a residue of said second polymeric material. For example, group X may be bonded to the polymer backbone of said second polymeric material.

30

Said subterranean formation suitably includes a production means, for example a production well, via which materials, for example organic fluids such as oil, may be removed

from the subterranean formation. Preferably, the subterranean formation is contacted with said third polymeric material upstream of the production means. Said subterranean formation may include one or more of said  
5 production means.

Said subterranean formation suitably includes a injection means, for example an injection well, via which fluid may be injected into the subterranean formation for driving  
10 materials within the formation towards said production means. Said subterranean formation may include one or more said injection means.

Said production means and injection means are suitably  
15 spaced apart across a reservoir which contains materials, for example, oil to be removed.

The process of said first and second aspects preferably includes the step of injecting a first injection fluid  
20 into the subterranean formation via said injection means. Said first injection fluid preferably includes a solvent which is preferably water. Said water may be derived from sea water.

25 A said first injection fluid may be prepared which comprises said third polymeric material and, after preparation, said first injection fluid may be injected into the subterranean formation. Alternatively, a said first injection fluid may be prepared which comprises said  
30 first and second polymeric materials and such a first injection fluid may be injected into the subterranean formation and arranged to produce said third polymeric material downstream of a position of injection of the

injection fluid into the subterranean formation.

Preferably, said first injection fluid which forms said third polymeric material in situ includes an acid and/or catalyst as described above to facilitate production of  
5 the third polymeric material.

Thus, said first injection fluid preferably carries the third polymeric material within the subterranean formation, whether the third polymeric material is  
10 produced prior to or after injection of the injection fluid into the formation.

Said first injection fluid is suitably arranged to have a viscosity (suitably when it comprises said third polymeric  
15 material) which is greater than the viscosity of water. The ratio of the viscosity of said first injection fluid (when it comprises said third polymeric material) to that of water may be at least 1.5, preferably at least 2, more preferably at least 3, especially at least 4. The ratio  
20 may be less than 100. Advantageous, the first injection fluid may be formulated with varying viscosities by varying the relative amounts and/or concentrations of the first and second polymeric materials used to prepare the third polymeric material. The viscosity of said first  
25 injection fluid (when it comprises said third polymeric material) may be less than 10 poise. Suitably, it is greater than 1 poise, preferably greater than 2 poise, more preferably greater than 3 poise, especially greater than 4 poise.

30

Said first injection fluid (suitably when it comprises said third polymeric material) is suitably arranged to lower the interfacial tension between water and oil.

Thus, the interfacial tension between water which may be used to drive materials to a said production means and oil in the absence of said third polymeric material may be less than in the presence of said third polymeric material.

Said first injection fluid is preferably injected into the formation at ambient temperature. It is suitably injected at a pressure below the fracture pressure of the formation.

After injection of said first injection fluid, a second injection fluid may be injected via said injection means into said formation. Said second injection fluid is arranged to contact the visco-elastic liquid of said first injection fluid and push the liquid and material contained within the formulation to a production well. Said second injection fluid may be selected from any such fluids known to those skilled in the art. For example it may comprise sea water or a gas such as carbon dioxide. Said second injection fluid suitably has a lower viscosity than said first injection fluid.

The invention extends to a formulation comprising:

- (a) said first polymeric material described above;
- (b) said second polymeric material described above;
- (c) water; and
- (d) a salt.

Said salt may be sodium chloride. Said water may be derived from sea water containing said salt. Said formulation preferably includes an acid, especially a protic acid.



The invention extends to a formulation comprising:

- (a) a third polymeric material described above;
- (b) water; and
- 5 (c) a salt.

Said salt and water may be as described above.

Any feature of any aspect of any invention described  
10 herein may be combined with any feature of any aspect of  
any other invention described herein mutatis mutandis.

Specific embodiments of the invention will now be  
described by way of example with reference to Figure 1  
15 which is a diagrammatic cross-section through a  
subterranean oil-bearing formation which includes a  
production and an injection well.

Referring to figure 1, there is shown a subterranean fluid  
20 (e.g. oil/gas) bearing formation 2, including gas  
reservoir 3, in which production wells (e.g. production  
well 4) having production perforations 6 has been formed.  
Formation fractures 8 which extend into the primary well  
are also shown. During primary production, natural  
25 pressures within the formation 2 force oil through rock  
pores into fractures 8 and into the production wells.

Injection wells 10 and associated injection perforations  
12, are drilled in the formation 2 for use in implementing  
30 secondary (and subsequent) recovery processes. In a  
secondary process water or steam may be injected into the  
injection well 10. The injected fluid passes through the  
injection perforations and into the oil bearing formation

2 whereupon it forces oil towards and into the production  
well 4.

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In a tertiary recovery process an aqueous polymer  
5 formulation, described further below, is injected into the  
injection well and caused to move towards the production  
well. The formulation has viscosity and other physical  
and chemical properties which enable it to aid the release  
of oil from within the oil bearing formation and  
10 facilitate the transfer of hydrostatic forces to the oil  
to enable it to be pushed to the production well.

The aqueous polymer formulation comprises 1,4-di(4-(N-  
methylpyridinyl))-2,3-di(4-(1-formylphenyl) butylidene and  
15 poly(vinyl alcohol). These two polymers are caused to  
react in an acid catalysed reaction and the reaction  
product exhibits the advantages of properties which enable  
oil to be released and pushed towards the production well.

20 Examples 1 to 3 describe the preparation of the butylidene  
polymer; a blend of the polymer with poly(vinylalcohol);  
and a reaction product of the two polymers.

Example 1 - Preparation of poly (1,4-di(4-(N-  
25 methylypyridinyl))-2,3-di(4-(1-formylphenyl)butylidene

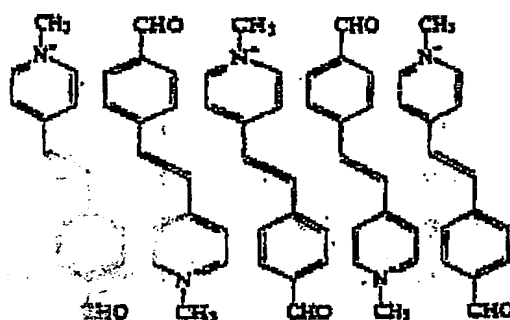
This was prepared as described in Example 1 of  
PCT/GB97/02529, the contents of which are incorporated  
herein by reference. In the method, an aqueous solution of  
30 greater than 1 wt% of 4-(4-formylphenylethenyl)-1-  
methylypyridinium methosulphonate (SbQ) is prepared by  
mixing the SbQ with water at ambient temperature. Under  
such conditions, the SbQ molecules form aggregates. The

solution was then exposed to ultraviolet light. This results in a photochemical reaction between the carbon-carbon double bonds of adjacent 4-(4-formylphenylethenyl)-1-methylpyridinium methosulphate molecules (I) in the aggregate, producing a polymer, poly (1,4-di(4-(N-methylpyridinyl))-2,3-di(4-(1-formylphenyl)butylidene methosulphonate (II), as shown in the reaction scheme below. It should be appreciated that the anions of compounds I and II have been omitted in the interests of clarity.

15

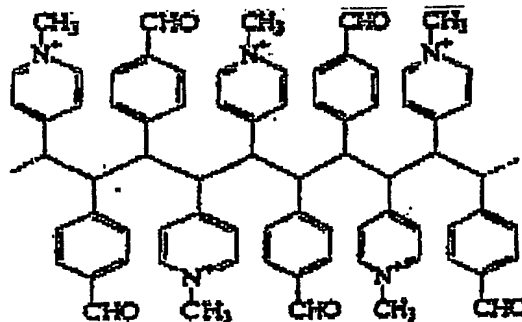
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I

> 1% w/w Aqueous solution  
UV irradiation



II

Example 2 - Preparation of polymer blend

A blend was prepared comprising 0.125 wt% of the butylidene polymer of Example 1 and 2 wt% of 88% hydrolysed poly(vinylalcohol) of molecular weight 300,000 in water. Suitably, the poly(vinylalcohol) is added slowly with constant stirring to an aqueous solution of the butylidene polymer so as to disperse the poly(vinylalcohol). Final dissolution may be achieved by maintaining the solution at a temperature of 60°C for a period of 6 hours.

Example 3 - Preparation of visco-elastic liquid

To the aqueous solution of the polymer blend described in Example 2 was added 0.01 wt% of 0.25M hydrochloric acid. This causes the butylidene and the poly(vinylalcohol) polymers to react according to the scheme below.

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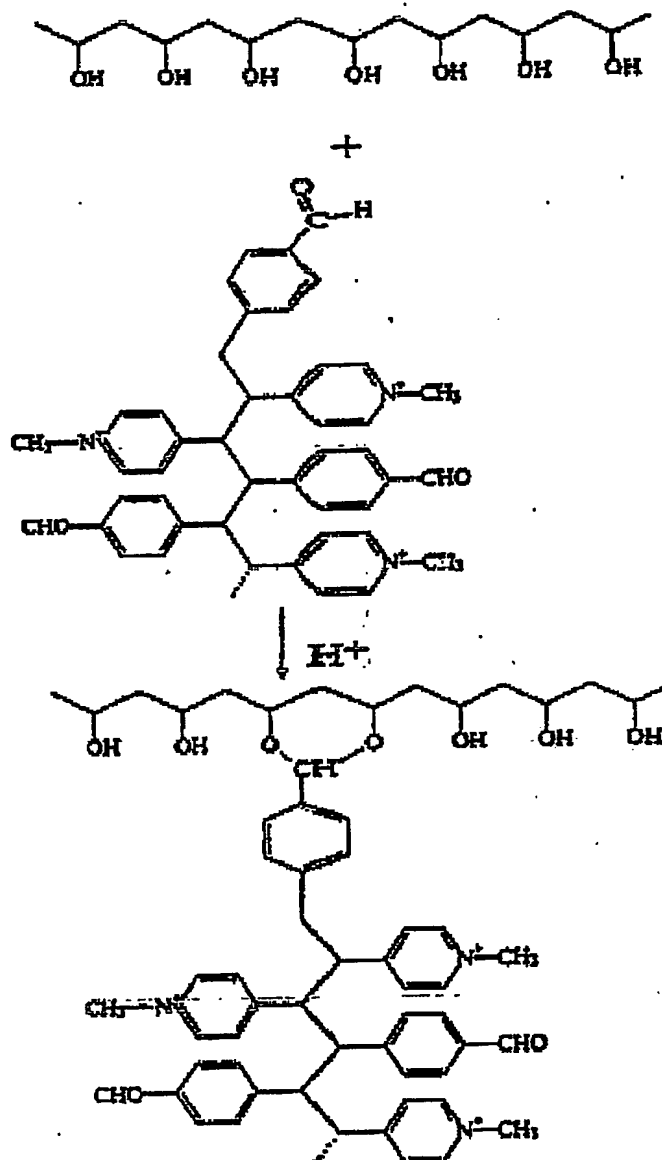
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30 The concentration of acid affects the speed of the reaction and therefore the development of the visco-elastic properties.

In a tertiary recovery process, the visco-elastic formulation may be prepared (so that the visco-elastic liquid of Example 3 is preformed) and, subsequently, it can be injected into the injection well in a conventional manner. The formulation is arranged to form a "squeeze" or a slug of material within the subterranean formation for example in oil-containing regions thereof. The squeeze has a greater viscosity than that of water and can have two effects: The first is that it can aid the release of oil from the formation by lowering interfacial tension; the second is that it can help the oil to be pushed out of the formation to the production well. As an alternative to the visco-elastic liquid being pre-formed a mixture comprising butylidene polymer, poly(vinylalcohol) and acid may be pumped into the injection well. During passage into the subterranean formation via the injection perforations, the reaction process takes place to form the visco-elastic solution in situ which can then release oil and enable it to be driven to the production well as described above. The oil is pushed to the production well by a fluid injected into the formation via the injection well after the visco-elastic formulation is in situ. The fluid may be sea water, carbon dioxide or any other available fluid.

25

It will be appreciated that subterranean formulations vary significantly from one to another. Advantageously, the visco-elastic formulations used can be tailored for use with any particular formation so as to optimise recovery of oil therefrom and minimise damage of the formation. For example the viscosity of the formulation may be adjusted by varying the relative amounts and/or concentration of the butylidene and poly(vinylalcohol)

30

polymers, and, in the case of the in situ formation of the visco-elastic liquid, the amount and/or concentration of acid may be adjusted to control the time taken for the visco-elastic liquid to form.

5

Examples 4 and 5 detail a simulation of the effect of use of the visco-elastic solution described.

Example 4 - Laboratory simulation of crude oil reservoir

- 10 A glass tube with sintered discs at each end, to which is applied a fluid flow, was constructed. Between the porous sintered discs was placed sand obtained from mainland UK which was taken to be representative of an unconsolidated sandstone type of formation.

15

The sand core was flooded with oil (obtained from the North Sea area) and left to stand for 24 hours.

All further tests were carried out at room temperature.

20

- After standing, potable water was applied to the system through the bottom end of the column by flowing through the sintered disc. As the water entered the bottom of the column the oil was forced up and out of the top. The removed oil was collected in containers of measured amounts. The flow of water was continued until the oil level in the water exiting the column was less than 5% by volume as seen from the level in the calibrated containers. The column at this point was still visually seen to contain oil, held on and between the sand grains.
- 25
- 30

To the water flow was added an aqueous solution of one-twentieth part of the column volume (to simulate the

formation of a "squeeze" referred to above) comprising 0.125wt% of the butylidene polymer of Example 1, 2wt% of the poly(vinylalcohol) described in Example 2 and 0.01 wt% of hydrochloric acid catalyst.

5

The aqueous solution described was applied at one tenth of the flow rate of the original water applied to the column. This rate was continued until the new fluid was thought to be 25% of the distance up from the bottom of the column,  
10 at which point the flow rate was increased until at 50% of the distance up from the bottom of the column, the flow rate was the same as the original applied water rate.

During the addition of the aqueous solution, oil was seen  
15 to separate from the sand on the walls of the glass column and flow upwards as a discrete band.

After one and a half volumes of the water volume calculated to be present in the column the oil content of  
20 the water leaving the column and being collected in measured amounts was seen to increase.

From an initial calculation of the original amount of oil placed in the sand column, less the amount found to be  
25 present in the recovered aliquots, there was a difference of around 25% of the original amount applied still present in the sand column.

A peak of oil content was found at about 4 volumes of the  
30 water content of the column. After this point the oil content dropped off markedly.



The total volume of oil removed from the column was calculated and found to be approximately 93% of the original volume of oil applied to the column.

5 Example 5

The procedure of Example 4 was followed except that the temperature of the arrangement was increased to 56°C. It was found that oil was recovered to the extent generally described in Example 4.

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Properties of the visco-elastic solution used in the oil recovery of Examples 4 and 5 include:

(a) It is stable in typical sea water obtained from the North Sea.

(b) It is not affected detrimentally by temperatures of 150°C and above.

(c) It is stable at temperatures below 0°C and may be prepared and/or applied in cold climates as well as hot.

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(d) It is not affected detrimentally by pressure of 7000 psi and above.

In oil recovery from a natural oil bearing formation, a flow of liquid from a suitable source (e.g. sea water) may be mixed with the three components described in Example 3 and the slightly viscous gel fluid can then be added to an injection well using appropriate pumping equipment. The flow rate of the fluid may be carefully controlled in dependence upon data collected from analyses of previous core samples, thereby to optimise the effectiveness of the oil recovery.

The exact composition of the formulation of the three components of Example 3 used may be varied depending upon the density and viscosity of oil being extracted; the density of water in the oil reservoir; the temperature and pressure in the oil reservoir; and the porosity and permeability of the oil bearing layers from which the oil is produced.

The visco-elastic solution may additionally be weighted (increased in density) for some applications by suspension in brine systems which may be included in formulations of three components to increase the density of the applied system thereby to further enhance the application and effectiveness of the chemicals used.

The reader's attention is directed to all papers and documents which are filed concurrently with or previous to this specification in connection with this application and which are open to public inspection with this specification, and the contents of all such papers and documents are incorporated herein by reference.

All of the features disclosed in this specification (including any accompanying claims, abstract and drawings), and/or all of the steps of any method or process so disclosed, may be combined in any combination, except combinations where at least some of such features and/or steps are mutually exclusive.

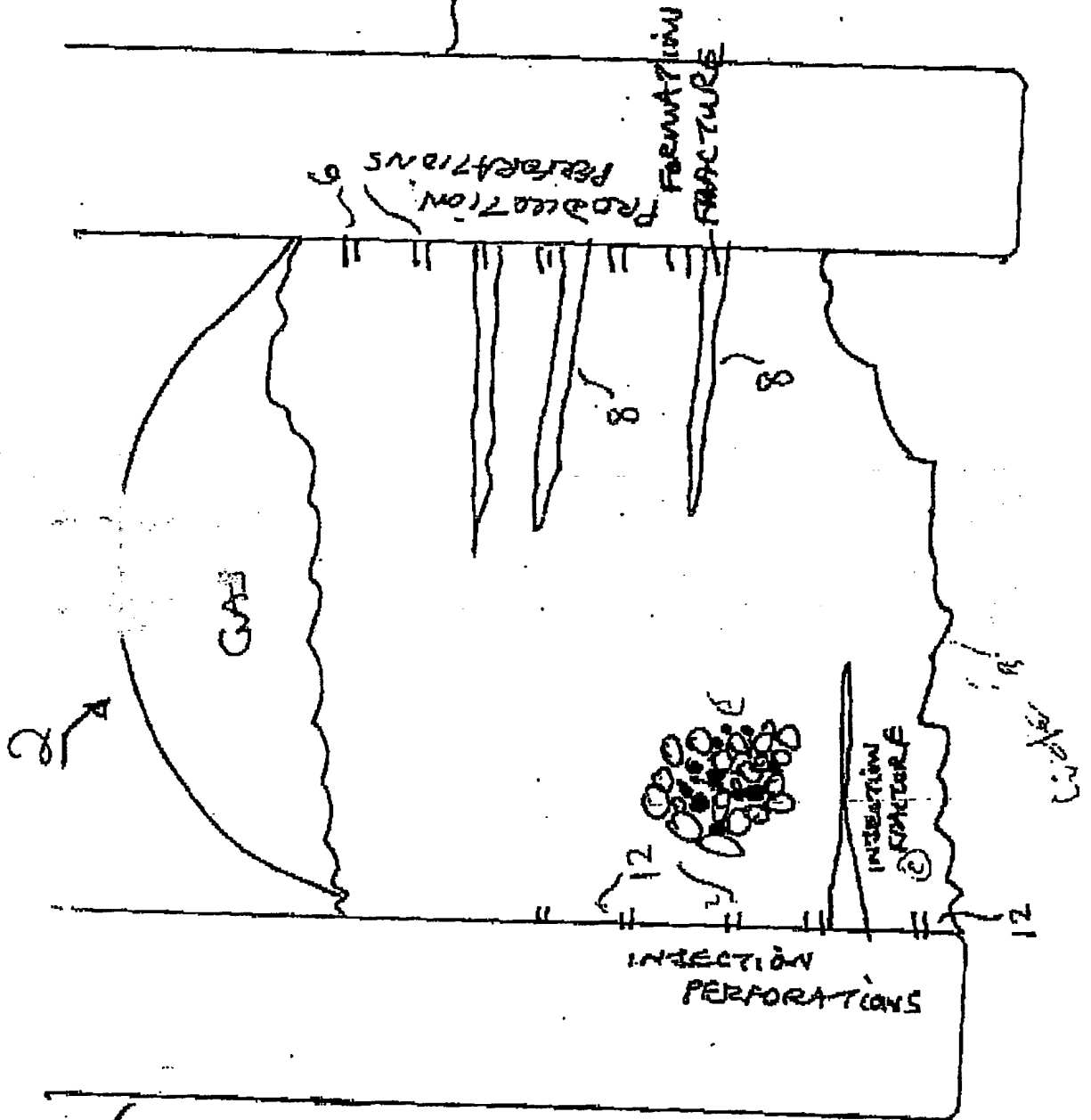
Each feature disclosed in this specification (including any accompanying claims, abstract and drawings), may be replaced by alternative features serving the same, equivalent or similar purpose, unless expressly stated

otherwise. Thus, unless expressly stated otherwise, each feature disclosed is one example only of a generic series of equivalent or similar features.

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- 5 The invention is not restricted to the details of the foregoing embodiment(s). The invention extends to any novel one, or any novel combination, of the features disclosed in this specification (including any accompanying claims, abstract and drawings), or to any
- 10 novel one, or any novel combination, of the steps of any method or process so disclosed.

Fig. 1.



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